

2019 Wastewater Collection and Treatment Report



CITY OF
SALMON ARM

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APPENDIX A Map 3.2 District of Salmon Arm Wastewater Collection System
Dayton & Knight (figure 4.1)

APPENDIX B Operational Certificate

1.0 Community General

The City of Salmon Arm is located in the southern interior of British Columbia on the southwest shoreline of the extensive Shuswap Lake system. With over 19,000 residents, Salmon Arm is the largest urban centre in the Columbia Shuswap Regional District. It serves as the commercial, cultural and administrative hub for an additional 35,000 residents of the Shuswap Lake region. Located at the junction of the Trans Canada Highway (TCH) and Highway 97B, Salmon Arm is a one-half day drive to Vancouver or Calgary and a 70 minute drive to Kelowna or Kamloops.

With a land base of 175 km², Salmon Arm is a relatively large municipality by area with most of the population concentrated within a few kilometers of the Trans Canada Highway and the downtown core. The surrounding terrain varies from the low lying marsh flats of Salmon Arm Bay to the extinct volcanic peak of Mt. Ida and the ridge lines of Fly Hills to the west and Larch Hills to the east. These highlands form the Canoe Creek and Salmon River watersheds which empty into Shuswap Lake. Sustainable land use planning over the years has resulted in the formation of an attractive, bustling, compact community surrounded by thousands of hectares of arable farmland, green space and natural shorelines.



Salmon Arm's commercial and industrial base is continuing to diversify. The housing market continues to remain tight. Retail, construction, professional services and healthcare, along with a wide array of entrepreneurial activities, are major sources of employment. Small businesses



flourish in Salmon Arm's business friendly environment. Key economic drivers are value-added wood processing, high tech and traditional manufacturing, tourism and agri-business. The continuing surge in construction activity points to a healthy market demand for new housing and floor space for commercial, industrial and institutional uses. The 2016 Census indicates a percentage growth in population of 1.2% from the previous 2011 Census. This compares to the provincial average growth of 5.6%.

1.1 Staffing

The City of Salmon Arm Engineering and Public Works Department is responsible for this municipal function. The Utilities Division is responsible for the operation and maintenance of the sanitary collection system and the Water Pollution Control Centre (WPCC) staff is responsible for the operation and maintenance of the Wastewater Treatment facility and the main lift Station located at Wharf Street. The WPCC is manned seven days of the week with 24-hour standby provisions for after hour alarm response.

Table 1 - Staff Overview

Engineering and Public Works	
Robert Niewenhuizen , A.Sc.T., Director of Engineering and Public Works	
Jenn Wilson , P.Eng., LEED® AP, City Engineer	
Utilities Division	
Gerry Rasmuson , B.Sc. <i>Utilities Manager</i> <ul style="list-style-type: none"> ◆ Level IV - Water Distribution ◆ Level IV - Wastewater Treatment ◆ Level I - Wastewater Collection 	Larry Kipp <i>Utilities Supervisor</i> <ul style="list-style-type: none"> ◆ Level I - Wastewater Collection
Mervin Arvay <ul style="list-style-type: none"> ◆ Level II - Wastewater Collection 	Devon Tulak <ul style="list-style-type: none"> ◆ Level I - Wastewater Collection
Ray Muller <ul style="list-style-type: none"> ◆ Level I - Wastewater Collection 	◆
Jason Baker <ul style="list-style-type: none"> ◆ Level I - Wastewater Collection 	Jason Philps <ul style="list-style-type: none"> ◆ Level I - Wastewater Collection
Water Pollution Control Centre	
Hart Frese <i>Chief Operator</i> <ul style="list-style-type: none"> ◆ Level IV - Wastewater Treatment 	Doug Stalker , Dip. Water Quality <i>Operator III</i> <ul style="list-style-type: none"> ◆ Level IV - Wastewater Treatment ◆ Level I - Wastewater Collection
Daryl Warnock , A.Sc.T., RSE, Dip. Water Engineering Technology <i>Operator III</i> <ul style="list-style-type: none"> ◆ Level III - Wastewater Treatment 	Damon Kipp , B.Sc., Dip. Water Engineering Technology <i>Operator III</i> <ul style="list-style-type: none"> ◆ Level III – Wastewater Treatment

2.0 Wastewater Treatment & Collection System History

2.1 Wastewater Collection System - History

The District of Salmon Arm and the Village of Salmon Arm amalgamated in 1971 to form the District Municipality of Salmon Arm on January 1, 1971, and then became the City of Salmon Arm in 2005. The Village was the original urban core area and sewer lines were installed during the 1930's to collect septic tank effluent and some crude wastes which were then discharged into an open ditch leading into Shuswap Lake. The surrounding District Municipality relied on septic systems as sewer collection was not an issue until the urban development of the Village overflowed into the surrounding Municipality. By 1964, the Village had initiated plans for sewage treatment

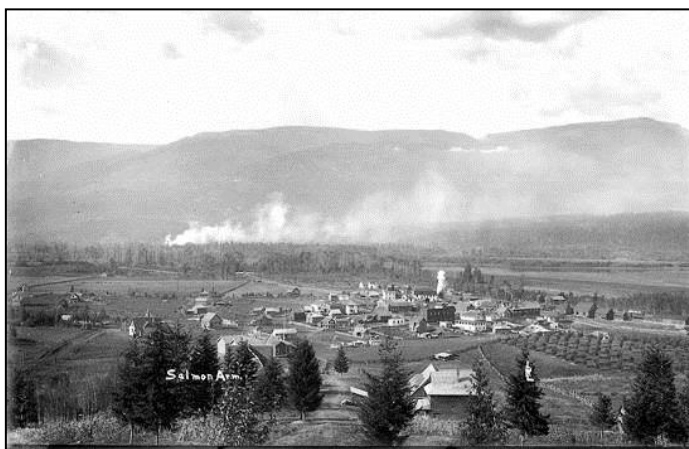


which included the construction of a lagoon along the waterfront for treatment. The lagoons would also service the Adams lake Indian Band lands. Concerned about the level of treatment that a lagoon offered, the Village decided to review their plans and objectives. By 1966, the review board recommended that the Village and District combine in their efforts to collect and treat wastewater. However, unable to agree upon implementation of various plans the Village applied to the Pollution Control Board for a permit to discharge highly treated effluent into Shuswap Lake. By the time this permit was granted in 1972, the Village



and District had amalgamated.

Ultimately the Engineering firm of Dayton and Knight Ltd were hired to undertake a Wastewater survey in 1972 to study various different treatment and effluent disposal methods. The Survey resulted in the construction and official opening of the existing Water Pollution Control Centre on May 14, 1977. Furthermore, the survey identified collection system priorities and set in motion the construction of the infrastructure that currently exists. The City's sewage collection and treatment systems have evolved into a well maintained collection system and a state of the art Wastewater Treatment Centre.



2.2 Wastewater Treatment Plant History

The original plant was constructed on the current site, 121 Narcisse Street NW, in 1977 after the proposed site at Minion Field, 2191 30th Street SW was rejected by the B.C. Agricultural Land Commission and Provincial Pollution Control Board. It was constructed at a cost of \$0.9 M and consisted of primary sedimentation, activated sludge, secondary clarification with chlorine disinfection. Solids were aerobically digested and stored in two 1 acre lagoons. Capacity of the plant was 3,000 m³ per day for a design service population of 6,250.

In 1982, phosphorus removal was added at a cost of \$0.1 M and consisted of precipitating phosphorus out of the effluent by the addition of ferrous chloride. Phosphorus was determined to be the limiting nutrient which contributes to the eutrophication and degradation of water quality in Shuswap Lake, particularly, Salmon Arm Bay. Currently the Salmon Arm WPCCC contributes less than 4% of the phosphorus loading in the bay.



Aerial Photo Stage IIIB prior to Landscaping

In 1986 the \$1.8 M Stage II Upgrade was the first major upgrade to the facility. The liquid process was altered from a common activated sludge process to an experimental trickling filter biological nutrient removal (BNR) system (Fixed Growth Reactor – Suspended Growth Reaction or FGR-SGR). As well, the aerobic digester was upgraded to an Autothermal Thermophilic Aerobic Digester (ATAD). Plant Capacity was increased to 3,500 m³ per day for a design service population of 8,750.

Improvements were made in 1991 to the solids process at a cost of \$0.5 M. The improvements consisted of changing aeration and solids pumping equipment. Rebuilding the ATAD tanks and added waste biological sludge thickening.

The Stage III Upgrade was split into two upgrades with the first part, Stage IIIA completed in 1998 at a cost of \$5.2 M. It consisted of improvements to the FGR- SGR process, new secondary clarifier, Supervisory Control and Data Acquisition system, increased ATAD capacity and biosolids dewatering. These improvements led to better control and monitoring, the ability to beneficially recycle biosolids and the decommissioning of the solids storage lagoons. Capacity was increased to 5,000 m³ per day for a design service population of 12,900. Stage IIIB was completed in 2005 without the Laboratory/Administration expansion. Of the \$7.4 M upgrade, \$2.3 M was funded by the Federal and Provincial Governments.

The upgrade consisted of a complete rebuild of the main lift station at Marine Drive with odour control, added redundancy to critical equipment, stand-by power, effluent filtration, replacement of the chlorination/de-chlorination system with Ultra Violet disinfection, an elaborate odour control system and architectural improvements to the original exterior of the original building.

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Capacity was increased to 6,700 m³ per day average flow for a design service population of 15,000. Stage IIIB was completed in 2008 with the \$0.4 M expansion of the Laboratory/Administration area. The Water Reclamation project was completed in 2010. This project utilizes the highly treated effluent for process water at the facility resulting in a 110 ML annual reduction in potable water use. In 2011, the Trickling Filter Media Upgrade was completed. The total cost of the project was \$0.55 M and entailed removing approximately 1,560 m³ of crossflow media and replacing with vertical flow media. This project was the result of the September 2007 pilot study (Dayton & Knight Ltd.) designed to reduce the impact of sloughing conditions problematic at the facility.



In 2017 an Engineering Audit was carried out on the WPC. The Audit concluded that the biological process is currently working well, with the plant showing very efficient removal of BOD, TSS and phosphorus. The plant is currently at about 90% of its 15,000 person equivalent projected design capacity, based on service population, which is projected to reach 15,000 people by between 2020 and 2025 based on current rates of growth. The design capacity of the plant is primarily based on biological and phosphorous loading to the plant, not flows. The primary trigger for plant upgrades will be the performance of the phosphorus removal process.

Based on the capacity assessment of the major plant unit processes, most have capacity well in excess of the 15,000 person equivalent design capacity. The unit processes with limited capacity and no redundancy include the anaerobic and anoxic reactors, which form part of the phosphate removal process. They currently have no redundancy, and are approaching their capacity limits.

The best estimate of when these capacity upgrades will be required is between 2020 and 2025 as the service population approaches 15,000 people; however, precise timing of upgrades is dependent on how the phosphorus removal process continues to perform. These upgrades are likely to be required in the next 5-10 years, with this in mind, the City began planning the Stage IV Plant Upgrades starting with a site selection study as per the City's Liquid Waste Management Plan in 2019.

Table 2 - Cost Summary Table

Project	Cost	Year
Stage I - 6,250 connected population	\$0.9 M	1977
Chemical Phosphorus Removal	\$0.1 M	1982
Stage II - 8,250 connected population	\$1.8 M	1986
Solids Improvements	\$0.5 M	1991
Stage IIIA - 12,500 connected population	\$5.3 M	1998
Stage IIIB – 15,000 connected population	\$7.4 M	2004
Laboratory/Administration Expansion	\$0.4 M	2008
Reclaimed Water	\$0.1 M	2009
Trickling Filter Media Upgrade	\$0.55 M	2011
UV System Upgrade	\$0.82 M	2018
Total	\$17.87 M	

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Estimated Insurable/Replacement Value (2018)	\$52 M	
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3.0 Wastewater Collection System

3.1 Overview of Collection System

The Utilities Division, through a schedule of systematic new improvements, upgrades and replacements strives to maintain and improve the sanitary sewer collection system. This Division plays an integral role in maintaining the health, safety and well being of the community. The sewer utility is a self-liquidating funded system which must provide for their own revenues through fees, taxes and other charges to support the expenditures required to operate and maintain infrastructure on a daily basis and long into the future.

3.2 Collection System

The City of Salmon Arm’s sanitary sewer collection system consists of 14 sewerage sub areas and 127 km of gravity and force main sanitary sewer pipes covering approximately 1800 hectares. There are approximately 6180 residential, commercial, industrial and institutional lots fronting onto the sanitary sewer system (2019 Court of Revision Report). There are seven (7) sewer lift stations that collect and pump sewerage to the Lakeshore Sewer Interceptor located on the foreshore where the main lift station, Wharf Street Pump Station, pumps the sewerage directly to the WPC (see Map 3.2). The Interceptor provides storage and flow equalization capabilities.

3.3 Lift Stations

All seven of the tributary Lift stations are inspected once a week by the City of Salmon Arm’s Utilities Division. All lift stations are thoroughly inspected and cleaned on a monthly basis. The stations are monitored using the City’s SCADA system which enables staff to troubleshoot and trend data on the system.

Table 3 - Wastewater Facilities

No.	Wastewater Lift Stations & Facilities	Address
1	Water Pollution Control Centre	121 Narcisse Street NW
2	Mosquito Park Lift Station	4290 Canoe Beach Drive NE
3	Clare's Cove Lift Station	5391-75 Avenue NE
4	Captain's Cove Lift Station	2251-73 Avenue NE
5	Canoe Beach Lift Station	7720-36 Street NE
6	Wharf Street Pump Station	1000 Marine Park Drive NE
7	Rotten Row Lift Station	681-10 Avenue SW
8	10 Avenue SW Lift Station	2270-10 Avenue SW [TCH]

3.4 Wharf Street Lift Station

The Wharf Street Lift station is gravity fed by the Lakeshore Interceptor. Three 30 Hp pumps with variable speed drives are used to feed the wastewater facility at rates determined by WPCC operators. The station was upgraded in 2002 with each pump rated at 80 liters/sec flow. The foul air is treated by utilizing ultraviolet light which catalyses the breaking of ambient oxygen and water vapor molecules into O⁺ and OH⁻ ions. These free radicals oxidize the odourous contaminants in the air. This reaction results in a sequential and instantaneous gas breakdown of the contaminants with minimal by-products, such as elemental sulfur, CO₂, water vapor, molecular oxygen and trace ozone. In the event of an extended power outage, there is the capability to connect the City's portable generator to the station to run the pumps. A second portable generator was purchased in 2011 primarily to service this critical lift station. This generator was utilized in July of 2012 when a primary Hydro feed to the electrical sub station failed resulting in a localized 33 hour power outage.



3.5 Lift Station Repairs and Modifications

There were no significant repairs or upgrades in 2019 besides the rebuilding of a pump at Wharf Street.

3.6 Sanitary Flushing

Approximately 16.5 km of sanitary mains were flushed in 2019 as part of the maintenance program. Certain main lines and services of concern are flushed quarterly.

3.7 Main and Service Interruptions

There were three mainline blockages within the sanitary collection system in 2019 and only a handful of service interruptions which are typically attributed to grease build up within the service pipe from homeowners or roots from nearby trees and shrubbery.

3.8 Inflow and Infiltration Monitoring Program

The program identifies locations where storm water or ground water enters the sanitary system. We continue to provide system improvements in an effort to reduce the amount of rainwater and groundwater entering the sanitary sewer system when it is cost-effective to do so. Reduction of Inflow & Infiltration (I&I) in the system lowers the risk of sanitary sewer overflows and can decrease the costs of conveying and treating wastewater.

3.9 Wastewater Collection Capital Projects

Table 4 - Capital Project Information

Capital projects completed in 2019
◆ Mosquito Park pump replacement
◆ Purchase new Sanitary pipe inspection camera
◆ Canoe 49 th St Sanitary main renewal
◆ SCADA upgrades
◆ Purchase Large Diameter Root Cutter
◆ Purchase new Hydro-Vac Truck
◆ TCH sanitary main renewal 4 th – 10 th St NE design
Capital Projects scheduled for 2020
◆ 75 th Ave NE Sanitary main renewal
◆ Canoe Beach Drive Sanitary main reroute
◆ TCH Sanitary lining 4 th – 10 th St NE
◆ Canoe – (TCH East – 63 rd) sanitary design
◆ Raven/Foreshore sanitary sewer renewal

4.0 Wastewater Treatment - Water Pollution Control Centre (WPCC)

The City of Salmon Arm WPCC is located at 121 Narcisse Street N.W. which is located west of the City’s Town Centre adjacent to the Shuswap Lake. This section of the report will detail the performance and operational strategies of the plant during the past year.



WPCC – After renovations



Wharf Street Lift Station

4.1 Process Overview

The process of wastewater treatment can be separated into two flow streams – liquid and solids also referred to as the liquid train and solids train.

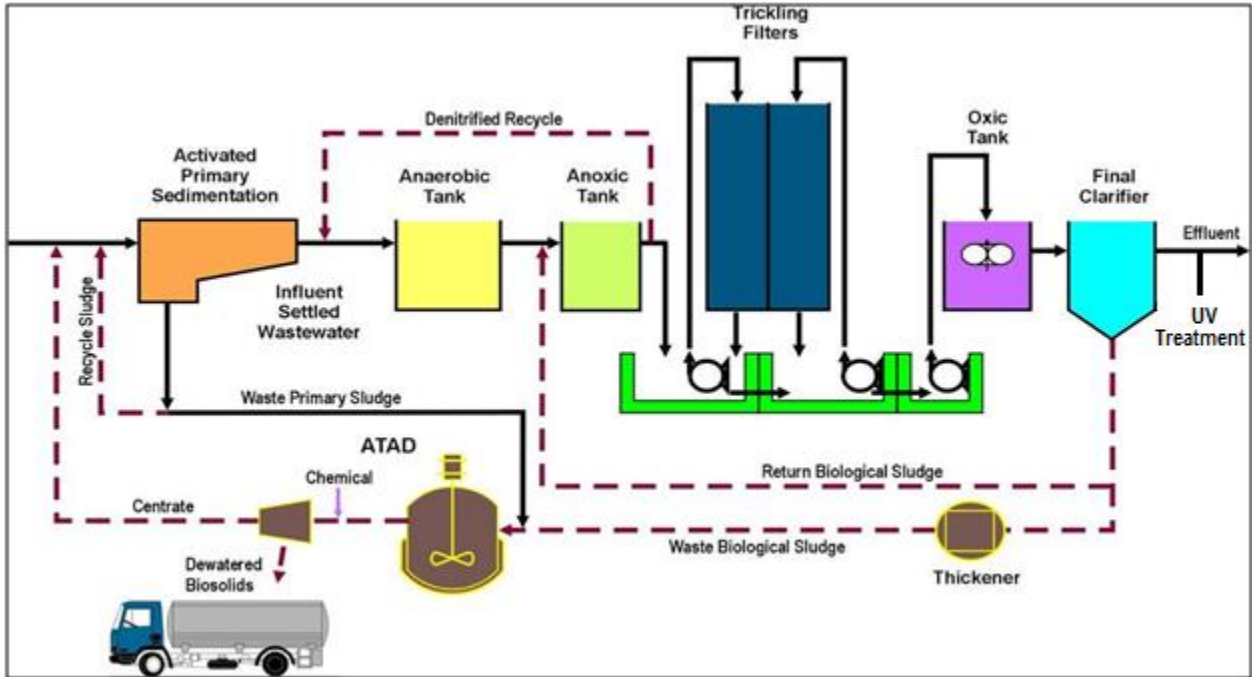


Figure 1: Wastewater Treatment Overview

Initially the wastewater is pumped into the plant from a sewage lift station (Wharf Street) located at Marine Park Drive. The influent then passes through several mechanical devices to remove large particles including rocks, rags, plastics and grit. This is done in the headworks of the facility and prevents damage to downstream equipment.



Headworks



Primary Sedimentation Tanks

The flow then enters one of two Primary Sedimentation Tanks where heavier organic and inorganic solids are settled out of the liquid stream. These particles are then pumped to the ATAD for stabilization. The liquid, on the other hand, then enters the tertiary BNR and SGR-FGR part of the facility for further treatment.



SGR's

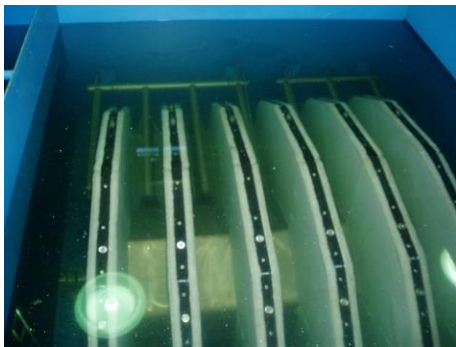


FGR

The tertiary treatment involves the use of bacteria to convert degradable organic matter into bacterial cells. These cells are then separated from the liquid in the secondary clarifiers.

The growth portion of the bacteria is removed from the process by thickening and pumped to the ATAD while the remainder is recycled back to the incoming wastewater. This is essential to maintain a balance of food (wastewater organics) to micro organisms.

The secondary effluent then passes through the Aqua Aerobics disk filtration system which provides 10 micron filtration. The effluent is then disinfected using a TrojanUV3000Plus™ Ultra Violet Light (UV) disinfection system prior to it being discharged into the Salmon Arm Bay in the Shuswap Lake.



Cloth Disk Filters



Secondary Clarifiers

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UV Treatment System



UV HMI

The primary solids and waste biological solids are digested (broken down) in the ATAD cells. This process uses high temperature bacteria (60 to 70 degrees Celsius) to stabilize and pasteurize the biosolids. Following processing, the biosolids are thickened with the use of high speed centrifuges and then hauled to landfill for potential site reclamation.



Centrifuge



Train B Odour Scrubber

Odour control is another major component of the plant operation. The odour control has been separated into two trains based on the concentration of odour generating compounds. One train deals with a large air volume of low odour concentration while the second train deals with a low air volume with a high concentration of odour compounds. The latter system uses a multi treatment system – biofilter, ozone contact, four (4) stage chemical scrubber and dilution while the other train uses a single stage chemical scrubber to oxidize the odour producing compounds.



Single Stage Chemical Scrubber



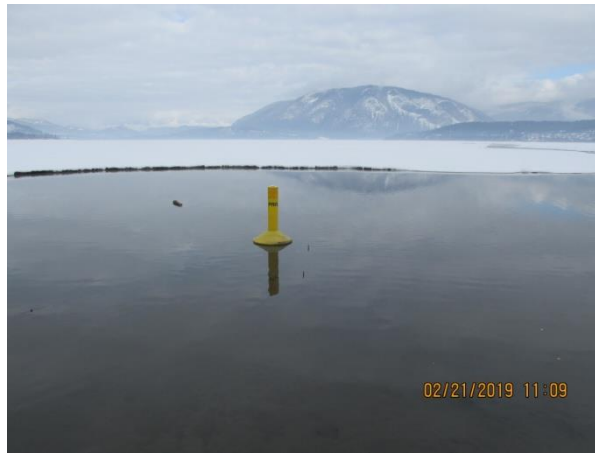
ATAD & Piping



Generator Set, Train B - Odour Control and Filtration Building

4.2 Flows

Plant flows decreased by 4.9% in 2019 from 2018. The average daily flow was 4,378 m³/d while in 2018 it was 4,605 m³/d. The highest flow of 5,398 m³/d was recorded on March 26 when rain accelerated the snow melt increasing the inflow and infiltration into the collection system.



Outfall with marker buoy

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Figure 2: Minimum, Maximum and Average Daily Flows

4.3 Nutrient Removal

Phosphorus concentration is the key nutrient contributing to poor water quality in the Salmon Arm Bay as it is in most lakes in British Columbia. The WPCCC contributed approximately 2.7% of the phosphorus loading to the Salmon Arm Bay in 2018. Additional information on the health of the entire Shuswap Lake is available from the **Summary: 2011–2013 Water Quality Monitoring Results for Shuswap and Mara Lakes** and can be viewed at:

https://www.fraserbasin.bc.ca/Library/TR_SLIPP/SLIPP_Water_Quality_Summary_2011_2013.pdf

Key points contained in the Summary are:

- The most significant source of phosphorus and other nutrients to the Shuswap and Mara Lakes is the Shuswap River. The Salmon and Eagle Rivers contribute the second and third largest loadings of phosphorus to the lakes.
- The largest non-point source of nutrients (over 95%) comes from seepage and run-off from agricultural lands in the Shuswap, Salmon and Eagle River watersheds. This source affects water quality in the lakes much more significantly than other sources do.
- If all wastewater treatment plants in the Shuswap increased their capability to tertiary treatment (some are now operating at secondary treatment levels), this would likely achieve the largest reduction in nutrients from a permitted point-source.
- Within Shuswap and Mara Lakes, the largest direct nutrient inputs occur naturally from decaying salmon following spawning.

Shuswap Lake Integrated Planning Process, "Summary: 2011–2013 Water Quality Monitoring Results for Shuswap and Mara Lakes" Pages 9, 10

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Table 5 – Phosphorus Mass Loading to Salmon Arm Bay from Salmon River, White Creek, Tappen Creek and Salmon Arm WPCC at 2019 Concentration and Flow – Daily Annual Averages

Total Mass Load (kg/d)	Salmon River* 1985 - 1999		White Creek* 1987 - 1990		Tappen Creek* 1988 - 1990		WPCC Year 2019	
	(kg/d)	% of Total	(kg/d)	% of Total	(kg/d)	% of Total	(kg/d)	% of Total
75.0	65.7	87.6%	6.9	9.2%	0.9	1.2%	2.1	2.0%

• *Data supplied from WPCC Outfall Impact Study, August 2002 (Dayton & Knight Ltd.)

Table 6 - Effluent Quality Summary - Yearly

Parameter (mg/l)	2011	2012	2013	2014	2015	2016	2017	2018	2019	OC
Flow (m ³)	4406	4382	4318	4355	4388	4406	4528	4605	4378	8200
Total Phosphorus (mg/l)	0.35	0.58	1.13	0.77	0.25	0.22	0.32	0.45	0.35	0.5
Kg P per Day	1.54	2.55	4.88	3.35	1.09	0.95	1.47	2.05	1.52	4.1
Kg P per Year	563	931	1781	1224	397	347	536	749	556	1497
Suspended Solids (mg/l)	7.9	7.4	7.2	5.4	4.4	4.8	5.6	7.0	5.9	20.0
BOD ₅ (mg/l)	4.8	7.5	6.5	8.3	5.8	6.7	8.7	9.1	9.7	15.0
Ortho Phosphorus (mg/l)	0.04	0.11	0.51	0.32	0.04	0.03	0.10	0.14	0.04	N/A
Ammonia (mg/l)	10.4	4.5	6.6	9.4	5.5	7.0	9.4	11.2	10.5	N/A
Nitrate & Nitrite (mg/l)	6.7	8.7	8.8	8.3	10.8	11.6	10.9	9.1	8.3	N/A
NH ₄ NO ₃ NO ₂ (mg/l)	16.7	13.1	15.4	17.0	16.3	18.4	20.1	20.6	20.6	N/A

Table 7 - Effluent Quality Summary - Weekly

Test Data	S.S. mg/l	BOD mg/l	Ortho P mg/l	Total P mg/l	NH ₄ mg/l	NOx mg/l
January 3, 2019	4.5	8.0	0.05	0.296	18.5	9.0
January 10, 2019	4.1	5.3	0.05	0.293	19.0	8.9
January 17, 2019	3.4	4.6	0.05	0.248	16.0	5.4
January 24, 2019	2.9	5.6	0.06	0.281	19.4	9.6
January 31, 2019	4.0	7.0	0.07	0.298	N/A	5.2
February 7, 2019	5.0	8.2	0.07	0.321	N/A	6.5
February 14, 2019	4.4	10.1	0.06	0.310	N/A	3.8
February 21, 2019	5.9	10.0	0.09	0.399	N/A	3.1
February 28, 2019	7.9	13.4	0.10	0.450	N/A	6.4
March 7, 2019	10.0	16.4	0.14	0.577	N/A	3.0
March 14, 2019	9.7	18.8	0.13	0.492	16.2	2.4
March 21, 2019	34.0	18.5	0.10	0.599	24.4	3.3
March 28, 2019	8.3	11.7	0.28	0.720	22.4	3.1
April 4, 2019	8.3	3.8	0.21	0.582	27.6	1.3
April 11, 2019	15.5	19.1	0.20	0.815	25.2	3.1
April 18, 2019	15.6	20.2	0.19	0.827	N/A	8.4
April 25, 2019	4.9	8.8	0.14	0.407	12.2	9.4
May 2, 2019	4.3	7.6	0.07	0.265	9.6	7.8

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Test Data	S.S. mg/l	BOD mg/l	Ortho P mg/l	Total P mg/l	NH ₄ mg/l	NO _x mg/l
May 9, 2019	5.8	8.2	0.14	0.357	11.2	6.3
May 16, 2019	8.2	8.7	0.12	0.428	N/A	9.0
May 23, 2019	5.4	7.6	0.14	0.346	N/A	9.0
May 30, 2019	6.1	7.8	0.07	0.320	7.4	8.2
June 6, 2019	6.8	8.0	0.07	0.341	9.1	9.5
June 13, 2019	6.6	8.4	0.10	0.323	3.4	15.8
June 20, 2019	5.1	8.0	0.10	0.267	2.6	10.2
June 27, 2019	1.9	7.0	0.03	0.182	3.2	15.2
July 4, 2019	0.5	6.7	0.05	0.189	5.1	10.2
July 11, 2019	1.4	7.4	0.09	0.194	4.8	8.1
July 18, 2019	2.5	7.1	0.03	0.199	5.8	13.3
July 25, 2019	4.3	8.5	0.04	0.237	5.9	10.3
August 1, 2019	3.2	6.6	0.05	0.228	7.5	12.3
August 8, 2019	3.2	6.4	0.03	0.222	7.0	11.1
August 15, 2019	4.0	8.2	0.02	0.258	8.5	7.8
August 22, 2019	4.4	8.0	0.02	0.252	10.7	8.3
August 29, 2019	2.8	8.1	0.05	0.297	8.7	6.9
September 5, 2019	3.3	7.7	0.06	0.250	7.5	8.2
September 12, 2019	3.8	9.9	0.03	0.228	6.5	7.4
September 19, 2019	4.2	9.0	0.05	0.250	4.9	7.8
September 26, 2019	4.1	9.4	0.03	0.263	5.5	15.3
October 3, 2019	4.6	9.1	0.04	0.270	4.3	11.3
October 10, 2019	6.9	9.8	0.07	0.375	7.9	9.4
October 17, 2019	6.9	12.7	0.07	0.403	11.7	7.1
October 24, 2019	4.9	13.2	0.03	0.286	5.5	12.7
October 31, 2019	5.0	12.1	0.04	0.286	8.7	14.1
November 7, 2019	7.3	11.6	0.07	0.414	6.0	13.5
November 14, 2019	2.8	11.9	0.05	0.292	6.8	13.9
November 21, 2019	3.6	11.7	0.06	0.369	13.1	7.5
November 28, 2019	5.4	14.7	0.11	0.326	11.2	8.4
December 5, 2019	5.7	12.8	0.05	0.312	15.0	8.3
December 12, 2019	6.5	15.2	0.06	0.371	11.8	11.2
December 19, 2019	5.5	14.8	0.06	0.324	10.6	8.9
December 26, 2019	N/A	N/A	N/A	0.266	N/A	N/A
Average	6.0	10.1	0.08	0.348	10.7	8.6
Maximum	34.0	20.2	0.28	0.827	27.6	15.8
Minimum	0.5	3.8	0.02	0.182	2.6	1.3

Table 8 - Tests performed by Caro Environmental Services on split sample.

Test Data	S.S. mg/l	BOD mg/l	Ortho P mg/l	NH ₄ mg/	NO ₃ mg/l	NO _x mg/l	E.Col	Fec. Col.
03-Jan	4.7	<6.0	N/A	11.4	4.80	6.24	3.6	3.6
10-Jan	4.8	7.0	0.0486	N/A	N/A	N/A	N/A	N/A
17-Jan	3.6	<8.7	0.0195	13.3	5.82	7.26	N/A	N/A
24-Jan	5.2	10.7	0.0477	N/A	N/A	N/A	N/A	N/A
31-Jan	3.2	<5.5	N/A	N/A	N/A	N/A	N/A	N/A
07-Feb	5.2	10.9	N/A	N/A	N/A	N/A	3.6	3.6
14-Feb	4.2	<6.5	N/A	19.7	N/A	N/A	N/A	N/A
21-Feb	6.0	8.3	0.0651	N/A	N/A	N/A	N/A	N/A

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Test Data	S.S. mg/l	BOD mg/l	Ortho P mg/l	NH ₄ mg/	NO ₃ mg/l	NO _x mg/l	E.Col	Fec. Col.
28-Feb	6.3	12.0	N/A	N/A	N/A	N/A	N/A	N/A
07-Mar	8.8	14.5	N/A	N/A	N/A	N/A	24000	24000
14-Mar	8.4	15.7	N/A	17.8	0.649	1.10	N/A	N/A
21-Mar	11.0	20.8	0.109	21.7	N/A	N/A	430	430
28-Mar	3.8	13.0	N/A	4.98	10.5	12.6	2400	4600
04-Apr	7.7	10.8	N/A	N/A	N/A	N/A	46000	46000
11-Apr	18.3	20.3	N/A	21.1	1.25	1.77	36	36
18-Apr	19.7	13.4	0.0567	N/A	N/A	N/A	9.1	9.1
25-Apr	5.4	<6.7	N/A	N/A	N/A	N/A	23	23
02-May	5.0	<2.0	N/A	N/A	N/A	N/A	23	23
09-May	5.8	<2.0	N/A	10.9	8.63	8.76	N/A	N/A
16-May	8.6	<5.7	0.0455	N/A	N/A	N/A	N/A	N/A
23-May	5.2	<8.0	N/A	5.32	N/A	N/A	3.6	3.6
30-May	4.6	<8.0	N/A	N/A	N/A	N/A	3.6	3.6
06-Jun	6.6	<8.0	N/A	5.44	12.2	12.9	7.3	43
13-Jun	7.8	6.9	0.018	N/A	N/A	N/A	<3.0	3.6
20-Jun	3.0	<6.7	N/A	N/A	N/A	N/A	N/A	N/A
27-Jun	2.8	<5.9	N/A	N/A	N/A	N/A	<3.0	<3.0
04-Jul	2.6	<6.8	N/A	3.59	9.66	11	N/A	N/A
11-Jul	<2.0	<6.7	0.0266	N/A	N/A	N/A	N/A	N/A
18-Jul	2.8	9.9	N/A	N/A	N/A	N/A	N/A	N/A
25-Jul	4.6	12.3	N/A	N/A	N/A	N/A	<3.0	3.6
01-Aug	3.2	<8.0	N/A	7.12	8.36	8.96	N/A	N/A
08-Aug	3.4	<7.1	0.0294	N/A	N/A	N/A	N/A	N/A
15-Aug	4.6	11.8	N/A	N/A	N/A	N/A	N/A	N/A
22-Aug	5.0	<7.4	N/A	N/A	N/A	N/A	9.1	9.1
29-Aug	3.6	<8.1	N/A	7.23	6.97	7.71	N/A	N/A
05-Sep	3.4	<7.2	0.0235	N/A	N/A	N/A	N/A	N/A
12-Sep	3.6	9.4	N/A	N/A	N/A	N/A	N/A	N/A
19-Sep	4.0	7.3	N/A	N/A	N/A	N/A	<3.0	<3.0
26-Sep	3.6	<6.5	N/A	3.39	9.61	10.9	N/A	N/A
03-Oct	4.2	<6.3	N/A	N/A	N/A	N/A	N/A	N/A
10-Oct	6.8	<6.8	N/A	N/A	N/A	N/A	N/A	N/A
17-Oct	8.8	8.9	N/A	N/A	N/A	N/A	N/A	N/A
23-Oct	3.8	<10.0	N/A	6.86	9.67	10.8	N/A	N/A
31-Oct	7.2	10.3	N/A	N/A	N/A	N/A	N/A	N/A
07-Nov	6.6	20.4	N/A	N/A	N/A	N/A	N/A	N/A
14-Nov	6.4	<7.2	N/A	N/A	N/A	N/A	N/A	N/A
21-Nov	7.2	20.7	N/A	7.42	6.65	7.89	N/A	N/A
28-Nov	7.2	7.9	0.0441	N/A	N/A	N/A	N/A	N/A
05-Dec	6.0	27.4	0.0150	N/A	N/A	N/A	N/A	N/A
12-Dec	7.0	9.0	N/A	N/A	N/A	N/A	3.0	3.0
19-Dec	7.6	7.5	0.0348	N/A	N/A	N/A	3.6	3.6
26-Dec	N/A	N/A	N/A	N/A	N/A	N/A	N/A	N/A
Avg.	5.9	9.7	0.042	10.45	7.29	8.30	N/A	N/A

4.4 Fecal Coliform

There were several unsatisfactory results in March and April with the ultraviolet disinfection system. The proprietary program controlling the system was modified and the issues were corrected and resolved.

4.5 Toxicity

As part of the Environment Canada's Wastewater Systems Effluent Regulations which came into effect January 1, 2013, the City was initially required to test the effluent for toxicity quarterly. However, having never failed a toxicity analysis, the frequency was reduced to annually. This was completed on effluent collected on December 10th, 2019 where once again analysis concluded that the effluent discharged from the facility is nontoxic.

4.6 Biosolids

The City of Salmon Arm produced approximately 350 dry tonnes of Class B biosolids during 2019. The biosolids are used by the Columbia Shuswap Regional District for local landfill reclamation. Testing of the biosolids by CARO Environmental Services for nutrients, metals and fecal coliform occurred on December 19th. Test results, once again, verified the biosolids produced by the Auto Thermophilic Aerobic Digester (ATAD) were of high quality managed under the Organic Matter Recycling Regulation.

4.7 Operating Certificate

The City operates the WPCP under Operating Certificate issued by the BC Ministry of Environment on June 1st, 2018. The certificate is attached as **Appendix B**.

In addition, The City's system must also comply with Environment Canada's Wastewater Systems Effluent Regulations. The goal of the Regulation is to standardize wastewater treatment across Canada. The Regulation specifies conditions to be met in order for the discharge of wastewater including setting limits on the concentration of deleterious substances that are authorized to be deposited, as well as requirements concerning effluent monitoring, toxicity, record keeping and reporting. Since the City's Operation Certificate is generally more stringent, only additional monitoring by an accredited laboratory and reporting is required to meet the Regulation.

4.8 Liquid Waste Management Plan

The City's Liquid Waste Management Plan (LWMP) was adopted by City Council on November 2, 2004 and was subsequently approved by the Ministry of Environment (MOE). One of the commitments contained in the approved LWMP was to carry out a LWMP update during 2009 to review progress, update the schedule, and make any required revisions in consultation with MOE. The City has been working with WSP Consulting Engineer to update LWMP. In the fall of 2010 meetings were held with MOE staff in an effort to review the proposed updates and amendments. Resulting from these discussions a draft LWMP update memorandum has been prepared and submitted for MOE review and comment.

4.9 WPCC Capital Projects

Table 9 – WPCC Capital Project Information

WPCC Capital Projects completed in 2019
◆ Stage IV Engineering Site Selection Study (Started)
Staff Initiated WPCC Projects Completed in 2019
◆ Upgraded Filtration Building Lighting to LED
◆ Purchase New Aerator for Oxidic Tank
◆ Instrumentation Improvements
WPCC Capital Projects scheduled for 2020
◆ Continue Stage IV Engineering Site Selection Study & Pre-design
◆ Activate Cell 6 Auto Thermophilic Aerobic Digester
◆ Upgrade Facility Lighting to LED

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APPENDIX A

